

About Us..

- **DVC Process Technologists** headquartered at Pune is a Technology & Innovation driven company that offers comprehensive processing solution for Edible Oil and Fats, Oleochemicals & Biodiesel industries.
- Serving the industry with dedicated team of technocrats and engineers with vast experience in Oils & Fats and allied industries
- Own **ISO Certified manufacturing facilities** near Pune at Supe & Jejuri with total work area of 40,000 Sqft & 22,000 Sqft respectively.



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Technology Offered

DVC is a single point solution provider for design, supply, installation & commissioning of process plant & equipment for :

- Vegetable Oil Refineries
- Oil mill Plants
- Fat Modification
- By-Product processing like Gums (Lecithin) Drying & Acid Oil.
- Integrated Biodiesel Production Plants for multiple feedstocks
- Solvent Extraction Plants & Flash Desolventization Plant
- Oleochemical Plants
- Technical Audits & Upgradation
- DVC Proprietary Equipment Designs like SCR® scraped surface heat exchanger, FEVAC® vacuum heater, REGV® regenerative vacuum heater, etc.
- Process & Tank Farm Automation
- · Skid mounted plants
- Zero Liquid Discharge Plant (ZLD)

Ongoing turnkey projects under execution

SL. NO.	LIST OF ONGOING PROJECTS	NAME OF CLIENT		
1	40000 Tons Tank farm Fabrication & Automation Turnkey Project	OLAM INTERNATIONAL Gabon, Africa		
2	Capacity enhancement of Degummed Soy Oil Refinery From 100 TPD to 200 TPD	Ruyat Oil Limited Lagos Nigeria		
3	50 TPD Soybean & Palm Oil refinery	OLEOS VEGETABLES Ecuador		
4	100 TPD & 250TPD Vegetable refining Plant	HUILERIE INDUSTERIAL DE TAMATARE (HITA), Madagascar		
5	100 TPD Soybean oil Refinery	DARSHANA SOLVANT, India		
6	50 TPD Soybean oil Refinery	VASUNDHARA, India		
7	500 TPD Soybean Oil Refinery (with dual scrubbing system for tocopherol rich stream)	GOYAL PROTEINS, India		
8	200 TPD Sunflower Oil Refinery	SET WAY INDUSTERIES, Ebene, Mauritius		
9	30 TPD Biodiesel Plant	BLUESTONE ENRGY, India		
10	Chicken Oil Refinery (Pilot scale)	GROWELL FEEDS PRIVATE LIMITED, India		

Recently delivered projects with capacity enhancement						
Sr No	LIST OF PROJECTS	NAME OF CLIENT				
1	150 TPD Refinery for Crude Palm & Rice bran Oil	MANTORA OIL PRODUCTS PVT. LTD India				
2	100 TPD Fish oil refinery	VINH PHUOC FOOD COMPANY LIMITED, Dong Thap Province ,Vietnam				
3	150TPD Multi-feedstock Biodiesel Plant	CHEMENERGY BIOFULES, India				
4	200 TPD Palm Oil Refinery	OLAM NIGERIA LIMITED, Lagos Nigeria				
5	200 TPD Crude Palm & Palm Kernel oil Refinery	JILNAS NIAGERIA LIMITED, Nigeria				
6	150 TPD Palm Oil Complex	QATAR FOOD INDUSERIES, Qatar				
7	Up-gradation of Palm Complex from 100 TPD to 150 TPD	OLAM PALM GABON, Africa				
8	Up-gradation of Palm Complex to 250 TPD	NILE AGRO INDUSTERIES Jinja, Uganda				
9	Up-gradation of Palm Complex from 60 TPD to 100 TPD	Olam PALM, Libreville, Africa				
10	Capacity Enhancement 300 TO 600 TPD	BUDGE BUDGE REFINERY ,India				

Soya Chunks - Introduction

- Soya chunks are made of soy flour, which is a by-product of soy oil extraction.
- Due to its good nutritive values it became popular all over the world.
- It has the similar protein equivalent to meat, and also similar chewy in texture.
- They are also free from cholesterol.
- These nuggets can be used in preparing various food products in households as well as in restaurants and can be important because of its high nutritional value.



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Flash Desolventisation System

- In conventional method of de-solventization process, the exposure of the de-oiled meal to direct heat (live steam) then to high temperature jacket heating do coagulate the protein present in de-oiled meal hence downing in the PDI value to 20-40. This low PDI meal is not suitable for the producing different products of Soybean required for the human consumption.
- The alternative process path for the de-oiled material leaving the solvent extraction process is a Flash de-solventising and cooling.
- Superheated solvent vapours are used for the Desolventisation of de-oiled wet meal providing the short contact time with heat. This prevents the reduction of PDI value.
- The meal obtained from FDS has PDI value in the range of **76 80** and hence the white flakes, which are produced by this method are raw material for producing the soybean protein concentrate and further downstream products in food industry.

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ypes Based on Protein Content:	Protein % (moisture free basis)
ull Fat Flour	39 - 42
efatted Flour (white flakes)	50 - 52
oy protein concentrates	65 - 68
ov protein isolates	~ 90





Production process for Soy Protein Concentrates

- In order to remove the water soluble sugars (carbohydrates), other low molecular weight soluble components and salts second stage extraction is done.
- The solvent used is a mixture of water and alcohol with the specific ratio of concentration. The solvent mixture concentration is adjusted such that the proteins are insoluble but the other products are soluble in the mixture.
- Depending on the extractability of the carbohydrates the ratio of ethanol and water is maintained between 70-30 and 60-40.



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Flakes (White)						Anna and a star of a second star
Flowrate	17 t/hr				Ma	Delence for
Moisture content	8.5%					ass balance for
Protein % on dry	0.8.8.9				Su	nar Extraction
basis	54%				00	
	-					
Screening		Fines 2.5	55 t/hr			
		N			Molasses 45% DS	
Extraction		IVIISCEITA 4-6% DS		Distillation	Protein	5-10%
Extraction				Distillation	Sucrose	40 - 45 %
	🖌 T I	Aqueous Ethanol 66	1%		Raffinose, stachyo	se 45-50%
					Ethanol	0.2-0.1%
Vet SPC 45% DS				Zam		
10001045/005						
*						
Stripping &	Stripping & Aqueous ethanol vapours		The second se			
Toasting						
	1					
		Cauda CDC				
•		Crude SPC	EF + /br			
Dryer Cooler		Crude SPC Flowrate 12. Moisture content 1	65 t/hr 42.	16 % of soybeans		
Dryer Cooler]	Crude SPC Flowrate 12. Moisture content 1	65 t/hr 42. 0.0% 74.	16 % of soybeans 4 % of flakes (white)		
Dryer Cooler		Crude SPC Flowrate 12. Moisture content 1 Protein Dry basis 0 Oil 0	65 t/hr 0.0% 59%	16 % of soybeans 4 % of flakes (white)		

Salient points for Sugar Extraction Process

- Temperature during Extraction : 65 70°C
- Pre soaking time : 20 minutes
- Extraction time : ~ 2.25 hours
- Bed Height : less than or equal to 1 meter.
- Ratio of Solvent to white flakes : 4.5 5.5 liters per Kg
- Ethanol & water Ratio : ~ 65 35

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Milling & Distillation - Sugar Extraction Process

- · Cleaner separates the hulls, impurities, stems, sticks
- Depending on the final application in the market the milling is done from 65 100 μ.
- In order to ensure prevention of bacteriological growth in the final product the moisture content is maintained below 8 %.
- Full miscella : 4 to 6 % dry solids (dissolved sugars & proteins)
- Optimized miscella concentration is around 5% for efficient extraction to maintain the Balance of SPC protein concentration & energy consumption.

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13